

Catalytic Hydrogenation of Olefins and Acetylenes over $C_{60}Pd_n$

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Organopalladium polymers of buckminsterfullerene, $C_{60}Pd_n$, catalyze hydrogenation of olefins and acetylenes at room temperature under a hydrogen atmosphere. The catalytic activity is mainly dependent on the ratio of C_{60} to Pd in the polymers. Partial hydrogenation of acetylenes is achieved by adding benzylamine as the cocatalyst.

Explosive studies on Buckminsterfullerene (C_{60}) and other spherical carbon clusters have provided us a number of fascinating physical properties and chemical reactivities of these new aromatic molecules.^{1,2)} In our previous paper, we reported a preparative route to organopalladium polymers, $C_{60}Pd_n$, as the first organometallic polymer of fullerenes, and referred to their catalysis toward heterogeneous hydrogenation of diphenylacetylene to 1,2-diphenylethane.³⁾ In this paper, we describe that the catalytic activity of $C_{60}Pd_n$ is dependent on the preparative route of the polymer, and successful hydrogenation of olefins and partial hydrogenation of acetylenes can be achieved with certain composition of $C_{60}Pd_n$.

Two methods were so far established to synthesize various composition of $C_{60}Pd_n$ as shown in Eqs. 1 - 2.³⁾ The reaction of C_{60} and $Pd_2(dba)_3 \cdot CHCl_3$ [dba = dibenzylideneacetone] can control the composition of C_{60} to Pd in the polymer by changing the charged ratios of C_{60} to the palladium precursor (Eq. 1). $C_{60}Pd_n$, where $n = 1 - 7$, were synthesized by this method. An alternative synthetic method for $C_{60}Pd_n$, where $n = 2 - 3$, is thermal disproportionation of $C_{60}Pd_n$ ($n = 1 - 2$) as shown in Eq. 2. On heating in refluxing toluene, palladium content in $C_{60}Pd_n$ became close to 2.5 - 2.7 and C_{60} was regenerated. Similar thermal disproportionation did not occur with $C_{60}Pd_n$ ($n > 3$). In contrast, we have now discovered that C_{60} reacted with $C_{60}Pd_n$ ($n > 3$) in boiling toluene to lower the palladium content as shown in eq. 3. In a typical example, a mixture of $C_{60}Pd_{3.37}$ (5 mg, 4.7 μ mol) prepared by Method A and C_{60} (11.5 mg, 16 μ mol) was heated in toluene under reflux for 5 h to give $C_{60}Pd_{2.84}$ (4.5 mg) and recovery of C_{60} (10 mg). Substantial change of the palladium contents was not observed with $C_{60}Pd_n$ ($n < 3$) under the same conditions.

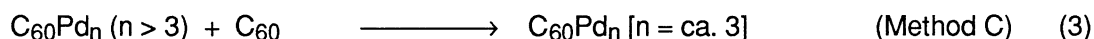
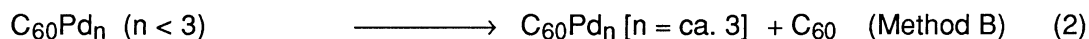
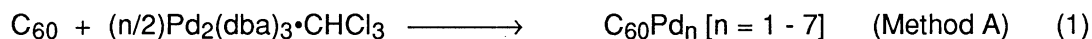


Table 1. Preparation of $C_{60}Pd_n$ and Catalytic hydrogenation of diphenylacetylene a)

Precursor	Method	Catalyst (mg) ^{b)}	$t_{1/2}$
$Pd_2(dba)_3 \cdot CHCl_3 + C_{60}$ (0.5 : 1)	A	$C_{60}Pd_{1.44}$	No reaction
$Pd_2(dba)_3 \cdot CHCl_3 + C_{60}$ (1.5 : 1)	A	$C_{60}Pd_{2.58}$	No reaction
$Pd_2(dba)_3 \cdot CHCl_3 + C_{60}$ (2.5 : 1)	A	$C_{60}Pd_{3.37}$	45 min
$Pd_2(dba)_3 \cdot CHCl_3 + C_{60}$ (5 : 1)	A	$C_{60}Pd_{6.99}$	13 min
$C_{60}Pd_{1.44}$	B	$C_{60}Pd_{2.46}$	No reaction
$C_{60}Pd_{2.58}$	B	$C_{60}Pd_{2.71}$	No reaction
$C_{60}Pd_{3.37}$	C	$C_{60}Pd_{2.78}$	330 min
$C_{60}Pd_{6.99}$	C	$C_{60}Pd_{4.23}$	20 min

a) Diphenylacetylene (1 mmol) was stirred in cyclohexane (10 ml) at room temperature under a hydrogen atmosphere. Amount of palladium in the catalyst is 1 mol% to diphenylacetylene.

b) The ratios of palladium and C_{60} in $C_{60}Pd_n$ were determined by the Elemental Analysis and EPMA.

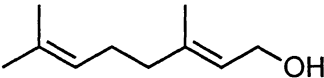
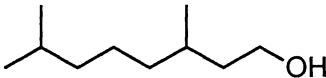
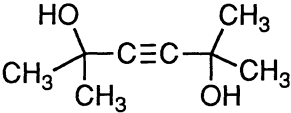
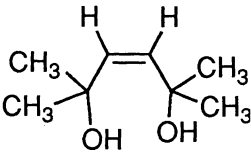
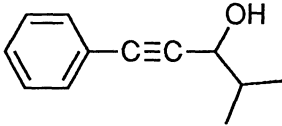
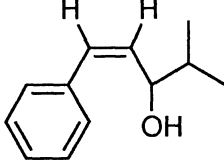
Hydrogenation over $C_{60}Pd_n$ was carried out in cyclohexane under a hydrogen atmosphere at room temperature. In Table I is summarized the catalytic activity as half-lives of the reaction with $C_{60}Pd_n$ prepared by the above three methods. The rate of the reaction was mainly dependent on the C_{60}/Pd ratio in the catalyst. Higher ratio of Pd to C_{60} in $C_{60}Pd_n$ resulted in the increase of the reaction rate in the case of $n > 3$. In contrast, $C_{60}Pd_n$ ($n < 3$) prepared by Method A or Method B was totally inactive. The catalytic activity of $C_{60}Pd_{2.78}$ or $C_{60}Pd_{4.23}$ prepared by Method C was lower than their precursors, $C_{60}Pd_{3.37}$ or $C_{60}Pd_{6.99}$, respectively.

We have pointed out in our previous paper, there would be two types of palladium atoms in $C_{60}Pd_n$; one is a binder of C_{60} , another is surface palladium atoms active for the catalytic hydrogenation.^{3,4)} The above results showed that the surface palladium atoms would exist in $C_{60}Pd_n$ ($n > 3$), but do not in $C_{60}Pd_n$ ($n < 3$). The reaction of C_{60} with up to 1.5 molar excess of $Pd_2(dba)_3 \cdot CHCl_3$ gave $C_{60}Pd_n$, in which all of the palladium atoms act as the binder of C_{60} . In increasing the ratio of the palladium precursor to C_{60} over 1.5, the surface palladium atoms are produced. Thermal disproportionation shown in Eq. 2 from $C_{60}Pd_n$ ($n < 3$) does not produce the surface palladium atoms. In contrast, the reaction of $C_{60}Pd_n$ ($n > 3$) with C_{60} shown in Eq. 3, which lowered the catalytic activity, suggests that a part of the surface palladium atoms reacted with C_{60} , giving rise to the conversion to the binder of C_{60} .

Catalytic hydrogenation of olefins over $C_{60}Pd_n$ ($n = 4.61$) also proceeded at room temperature under a hydrogen atmosphere. Ketones, esters, and aromatic rings were not hydrogenated under the conditions. The results are summarized in Table 2.

Interest in the hydrogenation of acetylenes is a possibility of partial hydrogenation of acetylenes to cis-olefins. A time-conversion plot of the hydrogenation of diphenylacetylene over $C_{60}Pd_n$ revealed the existence of cis-stilbene as an intermediate, suggesting the substantial rate

Table 2. Hydrogenation of olefins and acetylenes over $C_{60}Pd_n$ a)

Substrate	Method	Time	Product	Yield/%
diphenylacetylene	I	70min	1,2-Diphenylethane	91
	II	6 h	cis-stilbene	77 ^{b)} (95 : 0 : 5)
cyclooctene	I	3 h	cyclooctane	98(GC)
methylcyclohexene	I	160 min	methylcyclohexane	98(GC)
	I	24 h		83
PhCH=CHCH ₂ OAc	I	45 min	PhCH ₂ CH ₂ CH ₂ OAc	87
PhCH=CHCO ₂ Me	I	2 h	PhCH ₂ CH ₂ CO ₂ Me	95
PhCH=CHCOMe	I	80 min	PhCH ₂ CH ₂ COMe	80
	II	6 h		80 ^{b)} (96 : 4 : 0)
	II	6 h		76 ^{b)} (95 : 5 : 0)

a) Typical procedures; Method I. A mixture of $C_{60}Pd_{5.05}$ (1 mg, 4×10^{-3} mmol) and substrate (4.8×10^{-2} mmol) was stirred in cyclohexane (3 ml) under a hydrogen atmosphere. Method II. A mixture of $C_{60}Pd_{4.61}$ (3 mg, 1.15×10^{-2} mmol) and benzylamine (1.15 mmol) was stirred overnight under a hydrogen atmosphere. Then, a substrate (1.45 mmol) was added and the mixture was stirred for 6 h under a hydrogen atmosphere. It was confirmed that no substantial difference of the catalytic activity was observed between $C_{60}Pd_{4.61}$ and $C_{60}Pd_{5.05}$. b) Figures in parenthesis were the ratios among cis-olefin, trans-olefin, and alkane, respectively, determined by 1H NMR.

difference between the hydrogenation of diphenylacetylene to cis-stilbene and that of cis-stilbene to 1,2-diphenylethane. After screening of solvents and several cocatalyst, we found that the partial hydrogenation to cis-stilbene was achieved by the addition of amines in methanol. In Table II are shown three examples of partial hydrogenation of internal acetylenes over $C_{60}Pd_n$ ($n = 5.05$) in the presence of benzylamine.

Spherical carbon clusters (fullerenes) are large aromatic molecules having extensively delocalized π -electrons on their surface. Because of their spherical structure, the shape of π -orbitals is close to sp^3 rather than sp^2 . Catalysis of $C_{60}Pd_n$ is an interesting entry to understand the interaction of these characteristic π -orbitals on C_{60} with metallic species from synthetic organic chemistry. The above results suggest that features of $C_{60}Pd_n$ as the hydrogenation catalysts resemble the Lindler catalyst^{6,7)} or palladium on graphite⁸⁾ rather than Pd / C. In fact, the addition of benzylamine to Pd / C (5%) retarded the rates of hydrogenation of diphenylacetylene; however, hydrogenation to form 1,2-diphenylethane was seriously competed with the selective hydrogenation to stilbene. Selectivity of cis-stilbene formation is comparable or sometimes more excellent than the conventional catalysts.⁶⁻⁸⁾ These results suggest that the nature of C_{60} as a metal support is of interest in comparison with charcoal and graphite. Mechanistic studies and development of new catalysis are actively in progress.

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